# Optimization of Biological Aerated Filter and Microfiltration Operation for Wastewater Reclamation



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Typical Pressure Buildup Patterns

Typical Pressure Buildup Patterns

### A Wide Range of Potential Reuse Applications

King County (Seattle, WA) is studying whether to implement a water reuse program involving dispersed satellite treatment plants that may operate on a seasonal basis. Potential end uses include urban and agricultural irrigation, and less common applications such as wetlands creation, and direct or indirect streamflow augmentation to improve environmental conditions for fisheries recently listed under the Endangered Species Act. As shown in Table 1, the reuse applications have different water quality requirements, ranging from Washington's Class A reuse standards to high levels of nutrient and TOC removal.



2 NTU monthly average, 5 NTU maximum (WA Class A), anticipate adoption of CA Title 22 for membranes (0.2 NTU 95th percentile) Weekly Median

Washington Department of Ecology & Department of Health Class & standards for water reclamation and reuse

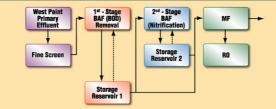
## **Project Background**

and Organic Toxics

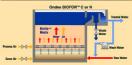
At a minimum, baseline processes must meet Class A water quality standards for oxidation, filtration and disinfection, Additional treatment could be required to meet more stringent nutrients, metals, organics, and turbidity levels. Following an in-depth screening of the individual treatment processes, two aerobic biological treatment trains were selected for testing in a nine-month pilot test. One uses a Biological Aerated Filter (BAF) and the other a Membrane Bioreactor (MBR) for wastewater oxidation. Other emerging technologies investigated for their small footprints and enhanced performance include Fuzzy Filter and ballasted flocculation (Actiflo and Densaded) for primary treatment. Fuzzy Filter and microfiltration (MF) for tertiary effluent filtration, and reverse osmosis for advanced treatment. This poster presents the results of the BAF-MF testing

#### **Pilot Testing**

2.2



#### **BIOLOGICAL AERATED FILTER (BAF)**



In this biological fixed film process, the primary effluent flows upward through a bed of filter media with aeration to create an aerobic environment. The biomass attached to the filter media removes soluble pollutants biologically, and insoluble pollutants are removed physically by filtration.

#### MICROFILTRATION (MF)



Microfiltration membranes are used for physical separation of small particles from liquids. They are designed to operate in a pressure or vacuum mode. Microfiltration membranes can be designed as hollow fibers or plates. depending on the manufacturer and application, and can be used for direct filtration of secondary effluent or as pretreatment for reverse osmosis membranes

#### PERFORMANCE GOALS

		B
BAF #1	BAF #2	П
<20 mg/L	<10 mg/L	ı
<20 mg/L	<10 mg/L	1
N/A	<2 mg/L	
	<20 mg/L <20 mg/L	<20 mg/L <10 mg/L <20 mg/L <10 mg/L



- Effluent turbidity < 0.2 NTU, 95th percentile, to meet anticipated Class A requirements.
  - Effluent TOC <2 mg/L, 50th percentile, to meet anticipated direct groundwater recharge criteria.
  - System Recovery >90%

#### **Test Results**

#### **BIOLOGICAL AERATED FILTER (BAF)**

#### Performance Optimization

- The BAF performance was optimized by varying the organic and hydraulic loading, and by adjusting the backwash frequency.
- Backwash frequency was adjusted by observing pressure buildup pattern and effluent turbidity. If the pattern exhibited a plateau and a turbidity breakthrough during the filter run (Pattern A), then the backwash frequency was increased. The backwash frequency was deemed optimized when pressure built up linearly (Pattern B) without a turbidity spike during the filter run.

#### Summary of Performance Loading for 1st Stage BAF After Optimization at Ontimized Performance

	BAF #1 Effluent	
CBOD, mg/L	29.4 (19)	9.2 (7)
TSS, mg/L	31 (25)	22 (9)
NH4-N, mo/L	12.8	1.57 (0.24)

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	Pilot Study Conclusion (Temp @ 10°C)	Manufacturer Suggested Range (Temp @ 25°C)	
Hydraulic ceding, gpm/ft <sup>p</sup>	3.3	1.6 to 8.2	Hydraulic Loading gpm/th <sup>o</sup>
CBCO Loading lb/kcf/d	297	376	CBOD Loading lb/kcf/d
TSS Loading. Ib/kctld	193	313	TSS Load ng. IbRc51d
			NH4-N Loading.

### Loading for 2<sup>nd</sup> Stage Nitrifying **BAF at Optimized Performance**

	Pilot Study Conclusion (Temp @ 10°C)	Manufacturer Suggested Ran (Temp @ 25°C
Hydraulic Loading gpm11 <sup>o</sup>	4.5	1.6 to 8.2
CBOD Loading lb/kcf/d	85	188
TSS Load ng. Ib/kcl/d	110	188
NH4-N Loading. Ib/kct/d	35	100

#### MICROFILTRATION (MF) **Typical Filter Runs**

- **Operating Data**
- Filtrate Flow: 6 nnm Feed Temperature: 12°C
- Temperature Corrected Flux (20°C); 28 gallons per day per sg. ft.

# Measured Performance

- Turbidity Removal: 0.06 NTU (95th Percentile)
- Filtrate TOC: 7.5 mg/L (50th Percentile)
- System Recovery: 89.5% (Backwash Frequency 10 min.)

#### CONCLUSIONS

- The 2-stage BAF without MF cannot meet the Class A requirements. The 2-stage BAF provides level of treatment comparable to activated sludge, but with a much higher loading, hence smaller footprint.
- The 2-stage BAF process provided a consistently lowturbidity (<10 NTU) feed stream to the MF unit.
- The MF unit provided very good filtrate turbidity quality meeting the Class A Reuse requirements and a lowsolids feed stream for the reverse osmosis pilot unit.
- The MF unit did not meet the TOC removal goal for direct groundwater recharge (potable).